

Journal of Hazardous Materials B132 (2006) 232-236

Journal of Hazardous Materials

www.elsevier.com/locate/jhazmat

Integrated effects of selected ions on 2,4,6-trinitrotoluene-removal by O₃/H₂O₂

Yaoguo Wu*, Chenhui Zhao, Qiuhua Wang, Ke Ding

Department of Applied Chemistry, Northwestern Polytechnical University, Xi'an 710072, China Received 19 May 2005; received in revised form 14 September 2005; accepted 20 September 2005 Available online 2 November 2005

Abstract

Considering the components of 2,4,6-trinitrotoluene (TNT)-containing water, this paper aims to research the integrated effects of ions on TNTremoval by O_3/H_2O_2 through the selection of CO_3^- , $HCOO^-$, Cu^{2+} and Al^{3+} . In view of TNT-removal rate and its constant, we find that the test with HCO_3^- or $HCOO^-$ or Cu^{2+} results in lower TNT-removal rate and its constant than control test. Therefore, it may conclude that HCO_3^- or $HCOO^-$ and Cu^{2+} has a potential to inhibit the efficacy of O_3/H_2O_2 , and that their inhibitions increase with an order from $HCOO^-$ to Cu^{2+} and to HCO_3^- . However, Al^{3+} is an exception, because it has a potential to improve the efficacy. When the two selected ions coexist, HCO_3^- and $HCOO^$ inhibit the efficacy. The inhibition is greater than that of either one alone, and also greater than their sum, and thus the integrated effect of $HCO_3^$ and $HCOO^-$ follows the synergistic effect. The inhibition of Cu^{2+} and $HCOO^-$ coexistence also is greater than that either alone, but smaller than their sum, and thus their integrated effect follows the independent effect. The integrated effect of Al^{3+} and $HCOO^-$ follows the addition effect. © 2005 Elsevier B.V. All rights reserved.

Keywords: O3/H2O2; Ions; Removal rate; Removal reaction rate constant; Integrated effect

1. Introduction

Advanced oxidation processes are a new means of objective pollutant-removal for drinking water and wastewater [1], which generally can generate the hydroxyl radicals, and thus they are of efficiency. Therefore, ozone/hydrogen peroxide (O₃/H₂O₂) process is considered to have a strong ability to generate hydroxyl radical (OH[•]), and have a strong effect on pollutant-removal. Consequently, the process has a great priority over others in the large-scale water treatment plant [2,3]. Therefore, many researches have been conducted for the efficacy of O₃/H₂O₂ to purify water [4-8], and several ions found have a potential to affect the efficacy. HCO₃⁻ and CO₃²⁻ react with OH[•], and consume OH^{\bullet} to decrease the efficacy of O_3/H_2O_2 [5,9], and thus have inhibitions. But humic substances with low concentration and HCOO⁻ have enhancement [7,9]. The effects of these ions are from the studies with one component in drinking water treatment [10,11], and most of them are model micro-polluted water, but few are with wastewater treatment. In fact, a treated water is

0304-3894/\$ - see front matter © 2005 Elsevier B.V. All rights reserved. doi:10.1016/j.jhazmat.2005.09.041 of multi-components, which may also influence the generation or (and) lifetime of OH^{\bullet} , and even have interactions among these components, so multi-components may also affect the efficacy of O_3/H_2O_2 process and their mechanisms may be more complex. The effects of other ions of the treated water, especially the coexistence of multi-components on the pollutant-removal by O_3/H_2O_2 , attract more and more attention, because these are helpful to the study on O_3/H_2O_2 in future, and even to its practice in water treatment.

In this work, TNT in the explosive-wastewater is used as an objective pollutant and its removal rates and their reaction rate constants are employed to judge the efficacy of O_3/H_2O_2 process. Carbonate is a common chemical component in wastewater, and its concentration increases with organic substance removal generally. The water environment is anaerobic wholly or partly for low concentration of dissolved oxygen caused by the transferring and consumption of oxygen, and some organic substances are transformed into simple organic acid substances here [12]. On other hand, during the producing and manufacturing processes for the blasting powder, some simple organic acid matters and metal ions (such as Cu^{2+} and Al^{3+}) are also released into wastewater. Thus, carbonate is present in a certain content, HCOO⁻ also exists in explosive-wastewater absolutely.

^{*} Corresponding author. Tel.: +86 29 88488018; fax: +86 29 88493549. *E-mail addresses:* wuygal@163.com, wuygal@pub.xaonline.com (Y. Wu).

According to the relation between pH and carbonate in water [13], the most form of carbonate is HCO_3^- in the TNT model wastewater under pH 7.9. Based on these, HCO_3^- , $HCOO^-$, Cu^{2+} and Al^{3+} are selected to investigate their integrated effect on TNT-removal by O_3/H_2O_2 .

2. Experimental methods

2.1. Reagent

A series of chemicals were purchased from Xi'an chemical reagents company, Xi'an city, Shaanxi province, PR China. Their commercial and chemical names are listed in the following: 2,4,6-trinitrotoluene (TNT), NaHCO₃, Al₂(SO₄)₃, HCOOH, CuSO₄ and H₂SO₄ (density 1.84). All of these are of analytical grade.

2.2. Model TNT wastewater

Under 25 °C, the analytical pure TNT is dissolved in tap water to make model wastewater for testing. In the study, the initial mass concentration (C_0) is about 30 mg/L, and pH 7.9.

2.3. Apparatus, equipment and experiment process

2.3.1. Apparatus and equipments

XFZ-5BI type ozone generator (manufactured by Tsinghua University, China), Gas flow counter (manufactured by Xi'an Institute of Thermal Engineering, Shaanxi Province, China), D100B-type peristaltic pump (manufactured by Huxi instruments company, Shanghai, China) and pHS-3C type pH analyzer (manufactured by Leici Instrumental Factory, Shanghai, China).

2.3.2. Experiment process

The reactor is a 1000 mL jar. O_3 producer works firstly, and then moderates its amperage and oxygen gas intake pressure, until the concentration of O_3 is stabilized in the out-take gas. The out-take gas is mixed with the model wastewater in a reactor through an air-distributor, and H_2O_2 input by the peristaltic pump into the reactor and blended with model wastewater simultaneously. During the test process, the surplus out-take gas is mixed with $Na_2S_2O_3$ solution to decompose O_3 . A sample about 20 mL is taken every 8 min, and analyzed immediately for TNT and other components concentrations. Before analysis, we have adjusted pH of samples to 2 or so by H_2SO_4 (density 1.84) to reduce the effect of metal ions. In this paper, the mass concentration of ozone is 2.3566 mg/L and its flux is 0.05 m³/h, and O_3/H_2O_2 molecular ratio is kept at 2:1, unless particular declaration.

2.4. Analytical methods

The concentration of TNT is determined by the spectrometer method [14](GB/T 13903-95, China), O_3 concentration in the liquid is determined by the Karman-Indigo method [15]. pH is recorded by pHS-3C analyzer.

Kinetics of TNT-removal is determined from a plot of the natural logarithm of the TNT concentration as a function of time. Pseudo-first-order rate constants (k) are determined by regression analysis.

3. Results and discussion

3.1. Integrated effect of HCO₃⁻ and HCOO⁻

To research the integrated effect of HCO_3^- and $HCOO^$ on TNT-removal by O_3/H_2O_2 , four reactors filled with 800 mL model wastewater are prepared firstly, and then on the test design, HCO_3^- is added to one, $HCOO^-$ to one, HCO_3^- and $HCOO^-$ to another one, and the other one is controlled as blank test. The results of these tests are shown in Fig. 1.

Compared with the control test, the presence of HCO₃⁻ or HCOO⁻ in the wastewater is of no good to TNT-removal, and decreased TNT-removal rates in certain degree respectively (Fig. 1). Thus, both of HCO₃⁻ and HCOO⁻ inhibited TNTremoval by O_3/H_2O_2 . Compared the two anions, HCOO⁻ inhibited TNT-removal more strongly than HCO₃⁻. HCO₃⁻ had a small inhibition, which was coincided with results of the studies by [5,6]. When the two anions coexisted, TNT-removal rate descended much more than either one. When the tests lasts for 24 min, compared with the control test, TNT-removal rate decreases about 23.2% by the two components coexistence. The decrease is greater than each of HCO_3^- (1.3%) and $HCOO^-$ (13.6%) respectively, and also greater than the sum of the decreases of HCO_3^- and $HCOO^-$ (1.3 + 13.6 = 14.9%). Obviously, the integrated effect of HCO3⁻ and HCOO⁻ coexistence on TNT-removal by O_3/H_2O_2 , was not a simple addition of the two effects of HCO₃⁻ and HCOO⁻, but synergistic effect.

The contaminant-removal by O_3/H_2O_2 is caused from OH[•] in fact and OH[•] is produced from the reaction between O_3 and H_2O_2 [3]:

$$2O_3 + H_2O_2 \rightarrow 2OH^{\bullet} + 3O_2 \tag{1}$$



Fig. 1. Integrated effect of HCO_3^- (3.54143 mol/L) and $HCOO^-$ (0.0002 mol/L) on TNT-removal.

Table 1

Pseudo-first-order rate constants (k) of TNT-removal by O₃/H₂O₂ under conditions with several wastewater qualities

| Ions added to the wastewater | $K(s^{-1})$ | R (%) |
|---|-------------|--------|
| Blank test (control test) | 0.02366 | 0.9873 |
| HCOO ⁻ (0.0002 mol/L) | 0.01448 | 0.9910 |
| HCO ₃ ⁻ (3.54143 mol/L) | 0.02338 | 0.9920 |
| $HCOO^{-}(0.0002 \text{ mol/L}) + HCO_{3}^{-}(3.54143 \text{ mol/L})$ | 0.00941 | 0.9478 |
| HCOO ⁻ (0.0001 mol/L) | 0.02105 | 0.9924 |
| $HCOO^{-}(0.0001 \text{ mol/L}) + HCO_{3}^{-}(3.54143 \text{ mol/L})$ | 0.01326 | 0.9892 |
| HCO ₃ ⁻ (1.19048 mol/L) | 0.02359 | 0.9874 |
| $HCOO^{-}(0.0002 \text{ mol/L}) + HCO_{3}^{-}(1.19048 \text{ mol/L})$ | 0.01137 | 0.9635 |
| Cu^{2+} (0.03125 mol/L) | 0.00636 | 0.9876 |
| Cu ²⁺ (0.00313 mol/L) | 0.00117 | 0.9737 |
| $HCOO^{-} (0.0002 \text{ mol/L}) + Cu^{2+} (0.03125 \text{ mol/L})$ | 0.00450 | 0.9897 |
| $HCOO^{-}$ (0.0001 mol/L) + Cu ²⁺ (0.00313 mol/L) | 0.00923 | 0.9968 |
| Al ³⁺ (0.002016 mol/L) | 0.02393 | 0.9850 |
| $HCOO^{-} (0.0002 \text{ mol/L}) + Al^{3+} (0.002016 \text{ mol/L})$ | 0.01598 | 0.9584 |
| $HCOO^{-}$ (0.0001 mol/L) + Al ³⁺ (0.002016 mol/L) | 0.01925 | 0.9698 |
| Al ³⁺ (0.00806 mol/L) | 0.02422 | 0.9894 |
| $HCOO^{-}$ (0.0002 mol/L) + Al^{3+} (0.00806 mol/L) | 0.01440 | 0.9896 |
| | | |

When O₃ and H₂O₂ are supplied constantly, and their concentrations are unvarying. Thus, OH[•] concentration is also stable in the reactor. Under the study conditions, the contaminant degradation process followed pseudo-first-order dynamics [16–18], and the inhibition or promotion ability of each component can be measured by the decrease of pollutant-removal reaction rate constant. Kinetics of TNT-loss were determined from a plot of the natural logarithm of the TNT concentration as a function of time. Pseudo-first-order rate constants (k) were determined by regression analysis, and the results were shown in Table 1. Pseudo-first-order rate constant for TNT-removal in control test was 0.02366 s^{-1} (*K*₁₄), and in tests with HCOO⁻ or HCO₃⁻ were 0.02338 s^{-1} (*K*₁₃) or 0.01448 s^{-1} (*K*₁₂), respectively, and in test with both is 0.0094 s^{-1} (K₁₁). Obviously, $(K_{14} - K_{11}) > ((K_{14} - K_{12}) + (K_{14} - K_{12})) > (K_{14} - K_{13}).$ Therefore, whether HCOO⁻ and HCO₃⁻ are individual or coexistent, both of them have the inhibition influence on TNT-removal by O_3/H_2O_2 . And the inhibition of HCOO⁻ and HCO₃⁻ coexisted was greater than one of both, and also greater than the sum of their single potentials. The TNT-removal rates and their reaction rate constants of the tests under other



Fig. 3. Integrated effect of Cu^{2+} (0.03125 mol/L) and HCOO⁻ (0.00002 mol/L) on TNT-removal.

concentrations of $HCOO^-$ and HCO_3^- are shown in Fig. 2 and Table 1, respectively. Analyzed these data, the same regularities were drawn. Therefore, the integrated effect of these two components on TNT-removal by O_3/H_2O_2 is not a simple addition of their single effects, but obeyed synergistic effect.

3.2. Integrated effect of Cu^{2+} and $HCOO^{-}$

The preparation is described in Section 3.1 mostly to study the integrated effect of Cu^{2+} and $HCOO^{-}$ on TNT-removal by O₃/H₂O₂, and Cu²⁺ is used instead of HCO_3^{-} . The results of these tests are shown in Fig. 3.

In this test study, though the concentrations of Cu^{2+} and $HCOO^-$ were only 0.03125 and 0.00002 mol/L, respectively, compared with the control test, both of them also depressed TNT-removal in certain degree. For instance, when the test is being done for 24 min, TNT-removal rate is 44.9% in the control test, 14.2 and 30.3% in the test with Cu^{2+} and $HCOO^-$, respectively, and 11.1% in the test with Cu^{2+} and $HCOO^-$ coexisted. Compared with the control test, TNT-removal rates decrease about 30.7 and 14.6% by the presence of Cu^{2+} or $HCOO^-$ respectively,



Fig. 2. Integrated effect of HCO₃⁻ and HCOO⁻ on TNT-removal under the more concentrations.



Fig. 4. Integrated effect of Cu^{2+} (0.00313 mol/L) and HCOO⁻ (0.00001 mol/L) on TNT-removal.

and depress about 33.8% by the presence of Cu^{2+} . Obviously, Cu^{2+} also inhibited TNT-removal by O_3/H_2O_2 , and the inhibition is much stronger than that of HCOO⁻ or HCO₃⁻. The integrated effect of Cu^{2+} and HCOO⁻ inhibited TNT-removal as the one of HCO₃⁻ and HCOO⁻, and their integrated inhibition was between one of both and the sum of both inhibitions.

Pseudo-first-order rate constants are determined for the TNT-loss reactions in Fig. 3 by regression analysis, and shown in Table 1 too. Under the study conditions, pollutant-removal reaction rate constant of the control test is 0.02366 s^{-1} , the constants of the tests with Cu²⁺ or HCOO⁻ existed individually are 0.02366 and 0.01448 s^{-1} respectively, and the constant of the tests with their coexistence is 0.0045 s^{-1} . Compared with the constant of the control test, the constant lowered about $0.01730 \, \text{s}^{-1}$ for Cu^{2+} , $0.00918 \, \text{s}^{-1}$ for HCOO⁻, and $0.01916 \,\mathrm{s}^{-1}$ for their coexistence. In view of the pollutantremoval rate constant, whether HCOO⁻ and Cu²⁺ exist alone or coexisted, they always inhibited TNT-removal by O₃/H₂O₂. And their integrated inhibition is between one of both and the sum of both inhibitions. So did to the two ions with other concentrations (Fig. 4 and Table 1). The conclusion obtained in view of the constants is same as that obtained in view of the TNT-removal rates. Therefore, the integrated effect of Cu²⁺ and HCOO⁻ is as independent effect. That differ from the integrated effect of HCO₃⁻ and HCOO⁻. These lighted that the integrated effects of two different ions were diverse and their mechanisms may be complex.

3.3. Integrated effect of $HCOO^-$ and Al^{3+}

To study the integrated effect of $HCOO^-$ and Al^{3+} on TNTremoval by O_3/H_2O_2 , the preparation of the study is described in Section 3.1 mostly, and Al^{3+} is used instead of HCO_3^- . The results of the tests are shown in Fig. 5.

Under the study conditions, compared with control test, in view of TNT-removal rate, the followings are obtained: $(1) Al^{3+}$ here is found to exert enhanced effect on TNT-removal, and



Fig. 5. Integrated effect of Al^{3+} (0.02667 mol/L) and HCOO⁻ (0.00002 mol/L) on TNT-removal.

against not only the effect of the selected metal ion, Cu^{2+} , but also the other selected anions, HCO_3^- and $HCOO^-$. These maybe suggest that one selected ion has its own effect on TNTremoval by O_3/H_2O_2 . (2) TNT-removal rate in the test with selected ions Al^{3+} and $HCOO^-$ coexisted, is smaller than that in control test, likewise smaller than that in the test with Al^{3+} solely, but greater than that in the test with $HCOO^-$ solely. For instance, when the tests last for 32 min, the TNT-removal rate was 50.8% in control test, 51.8 and 35.3% in the tests with Al^{3+} and $HCOO^-$ solely respectively, 35.5% in the test with Al^{3+} and $HCOO^-$ coexisted. Obviously, Al^{3+} accelerated the efficacy of O_3/H_2O_2 and diminished the inhibition of $HCOO^-$, thus the removal rate in the test with Al^{3+} and $HCOO^-$ coexisted is greater than that for $HCOO^-$ existed.

Pseudo-first-order rate constants for the TNT-loss reaction in Fig. 5 determined by regression analysis are shown in Table 1 too. The TNT-removal reaction rate constant is $0.02366 \,\mathrm{s}^{-1}$ (K_{34}) for TNT-loss in control test, and 0.02393 s⁻¹ (K_{33}) and $0.01448 \,\mathrm{s}^{-1}$ (K₃₂) are in the tests with HCOO⁻ and HCO₃⁻ alone respectively, and $0.01598 \,\mathrm{s}^{-1}(K_{31})$ in the test with HCOO⁻ and HCO₃⁻ coexisted. Obviously, $(K_{34} - K_{33}) > 0$, the present of Al³⁺ is useful to TNT-removal, and enhanced the efficacy of O₃/H₂O₂. $(K_{34} - K_{31}) < (K_{34} - K_{32}) < 0$, and $(K_{34} - K_{31}) \approx (K_{34} - K_{32}) - 2(K_{34} - K_{33})$, exposed that their coexistence had a potential to inhibit TNT-removal. The integrated effect was smaller than that for HCOO⁻, and mostly equal to HCOO⁻ inhibition subtracted two times of the acceleration of Al³⁺. Therefore, the integrated effect of Al³⁺ and HCOO⁻ on TNT-removal by O_3/H_2O_2 is approximately considered as sum of their single effects, and is called the addition effect. The integrated effect was different from that for HCO₃⁻ and HCOO⁻ coexisted and Cu²⁺ and HCOO⁻ coexisted. These also exposed that multi-components had complicated effect on pollutantremoval by O_3/H_2O_2 , and their mechanisms were complex.

The tests on the integrated effect of $HCOO^-$ and Al^{3+} with other concentrations were conducted, the TNT-removal rates and reaction rate constants were shown in Fig. 6 and



Fig. 6. Integrated effect of Al³⁺ and HCOO⁻ on TNT-removal under the more concentrations.

Table 1. Analyzed these data, and the same conclusions were drawn.

From all the tests above, it is found that different type of ions have different effect, and the integrated effects of the selected ions coexisted are also different. Why these phenomena are caused needs to be studied in the future.

Acknowledgements

This research was sponsored by NWPU plan of outstanding scholar (2002), and important project on NWPU graduate design or dissertation (2004–2005).

References

- S.A. Ali, O₃/H₂O₂ treatment of methyl-*tert*-butyl ether (MTBE) in contaminated waters, Water Res. 35 (15) (2001) 3706–3714.
- [2] W.S. Himebaugh, Advanced oxidation of munitions in wastewater, Natl. Environ. J. 5 (6) (1995) 42–45.
- [3] W.H. Glaze, J.W. Kang, Advanced oxidation process description of a kinetic model for the oxidation of hazardous materials in aqueous media with ozone and hydrogen peroxide in semibatch reactor, Ind. Eng. Chem. Res. 28 (1989) 1573–1580.
- [4] J.P. Duguet, C. Anselme, P. Mazounie, Application of combined ozone hydrogenperoxide for the removal of aromatic compounds from groundwater, Ozone Sci. Eng. 12 (1990) 281–293.
- [5] Jun Ma, Fenghua Shi, Study on Removal of nitrobenzene in water by O₃/H₂O₂, Environ. Sci. 23 (5) (2002) 67–71.
- [6] J. Hoigne, H. Bader, The role of hydroxyl radical reaction in ozonation processes in aqueous solution, Water Res. 10 (1976) 377–386.

- [7] Staehelln Johannes, Holgne Jurg, Decomposition of ozone in water in the presence of organic solutes acting as promoters and inhibitors of radical chain reactions, Environ. Sci. Technol. 19 (1985) 1206– 1213.
- [8] Kasprzyk-Hordern Barbara, Ziolek Maria, Nawrocki Jacek, Catalytic ozonation and methods of enhancing molecular ozone reactions in water treatment, Appl. Catal. B: Environ. 46 (2003) 639–669.
- [9] W. Haag, C.D. Yao, Rate constants for reaction of hydroxyl radicals with several drinking water contaminants, Environ. Sci. Technol. 26 (1992) 1005–1013.
- [10] W.H. Glaze, J.W. Kang, The chemistry of water treatment process involving ozone, hydrogen peroxide and ultraviolet radiation, Ozone Sci. Eng. 9 (5) (1987) 335–352.
- [11] S.D. Lambert, N.J.D. Graham, B.T. Croll, Degradation of selected herbicides in low land surface water by ozone and ozone hydrogen peroxide, Ozone Sci. Eng. 18 (3) (1996) 251–269.
- [12] Xiheng Zhang, Anaerobic Treatment Engineering of Wastewater, China Press of Environmental Science, Beijing, 1995, 1–34.
- [13] Sugui Dai, Environmental Chemistry, Higher Education Press, Beijing, 2000, 102-112.
- [14] Lin. Yu, Standards of Water Quality Monitor and Analysis, China Press of Environmental Science, Beijing, 1995, 1–34.
- [15] H. Bader, J. Hoigné, Determination of ozone in water by the indigo method, Water Res. 15 (1981) 449–456.
- [16] P. Bose, W.H. Gaze, D.S. Massox, Degradation of RDX by various advanced oxidation processes: I. Reaction rates, Water Res. 32 (4) (1998) 997–1004.
- [17] P. Bose, W.H. Gaze, D.S. Massox, Degradation of RDX by various advanced oxidation processes: II. Organic by-products, Water Res. 32 (4) (1998) 1005–1018.
- [18] Hideo Utsumi, Youn-Hee Han, Kazuhiro Ichikawa, A kinetic study of 3-chlorophenol enhanced hydroxyl radical generation during ozonation, Water Res. 37 (2003) 4924–4928.